

A matter of scale? – (Industrial) combustion research from the lab to real-life application

IFRF Event “From lab scale to industrial combustion:
challenges for the scale up of experimental and
simulation approaches”

Jörg Leicher, Rouen/France, April 25th, 2023

Does size/scale matter?

Spoiler alert: Yes, it does!
At least in combustion...



Scales in stationary combustion applications

Residential/commercial

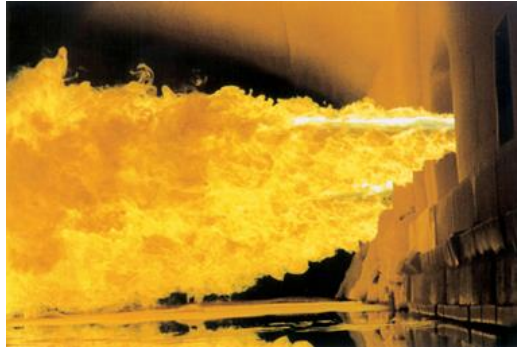
Source: Vaillant



- P: < **50 kW**, λ : 1.2 – 1.4
- Length scale: **1 m**
- Low-temperature heat, warm water
- Premixed or partially premixed combustion

Industrial process heating

Source: HVG



- P: up to **200 MW**, λ : 0.9 – 1.2
- Length scale: up to **100 m**
- Process heat
- Usually non-premixed combustion, often with air preheating or oxy-fuel

Power generation

Source: Siemens Energy



- P: up to **1.5 GW**, λ : ≈ 2
- Length scale: about **10 m**
- Power generation
- Lean premixed combustion (pressurized)

Similarity analysis in fluid dynamics

Similarity analysis and the use of **scaled-down models** have a long tradition in many fields of **applied fluid dynamics**.

Aviation



Image: WikiCommons/NASA



Image: KLM

Shipbuilding

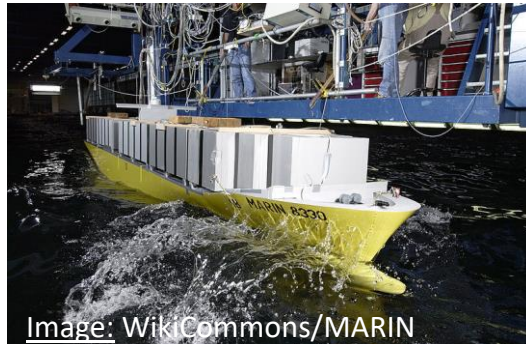


Image: WikiCommons/MARIN



Image: WikiCommons/Niels Johannes

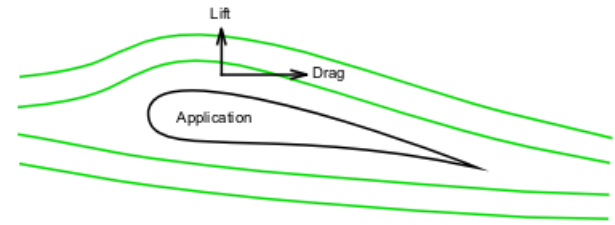
Criteria for similarity

Theoretically, there are three criteria needed to achieve complete similarity between a **reduced-scale model** and the **real-scale system** in a **non-reactive flow**: geometric, kinematic and dynamic similarity.

Geometric similarity: the **geometric model** is of the **same shape** as the application, usually scaled down.

Kinematic similarity: the fluid flows in both the model and the real application undergo **similar changes over time**, i.e. the **streamlines** are similar.

Dynamic similarity: the **ratios of all forces** acting on corresponding fluid particles and boundary surfaces in the two systems **are the same**.



Geometric Similitude:
Model is scaled.

Kinematic Similitude:
Fluid stream lines are scaled.

Dynamic Similitude:
$$\begin{pmatrix} \text{Lift (a)} \\ \text{Lift (m)} \end{pmatrix} = \begin{pmatrix} \text{Drag (a)} \\ \text{Drag (m)} \end{pmatrix} = \dots$$

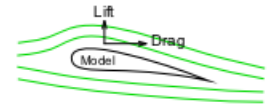
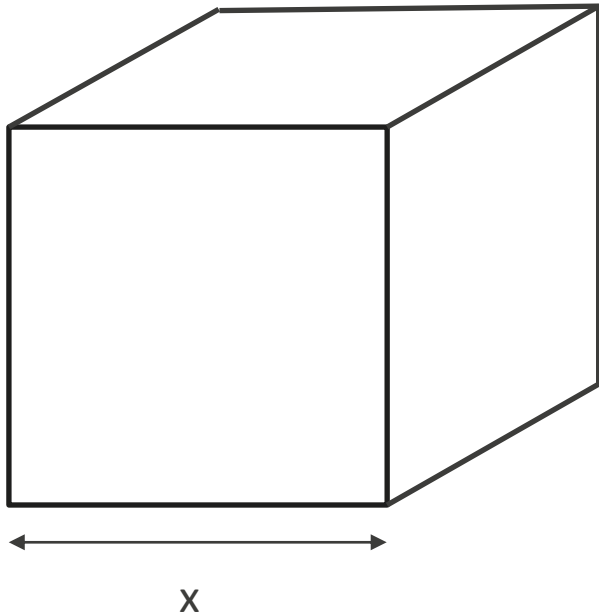


Image: [WikiCommons/Duk](#)

Criteria for similarity, cont'd

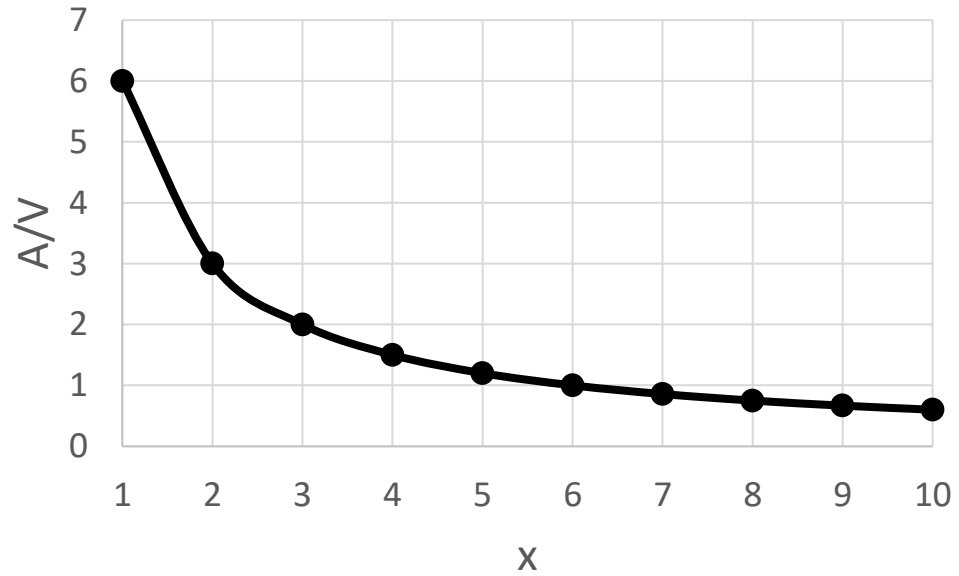
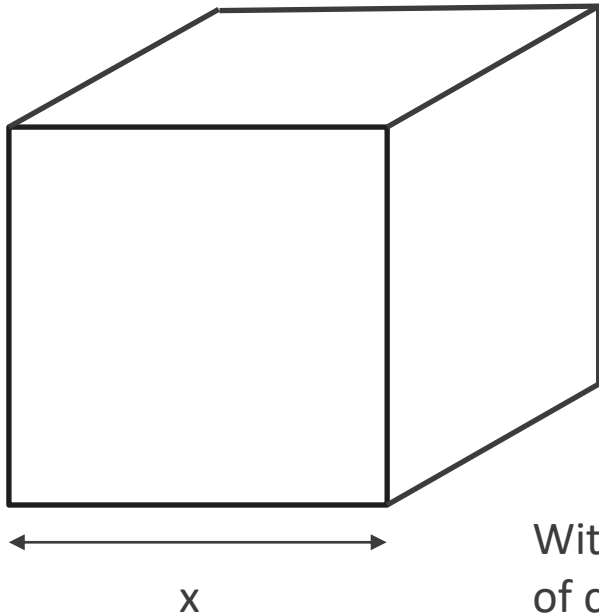
Theoretically, there are three criteria needed to achieve complete similarity between a **reduced-scale model** and the **real-scale system** in a **non-reactive flow**: geometric, kinematic and dynamic similarity.



- With **combustion**, things become a bit more difficult, as the fluid itself changes during the process (ρ , T , X_i , ...).
- Some **combustion-related phenomena** and aspects scale with the **volume** ($\sim x^3$) of the combustion space, e. g. heat release, chemical reactions or residence times.
- Others scale with the **surface area** ($\sim x^2$), most importantly wall heat losses.

Criteria for similarity, cont'd

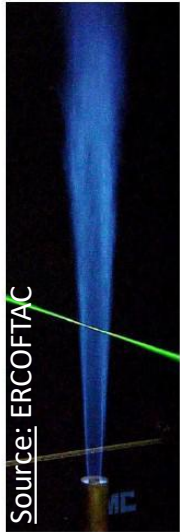
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With **combustion processes**, there is an additional layer of complexity.

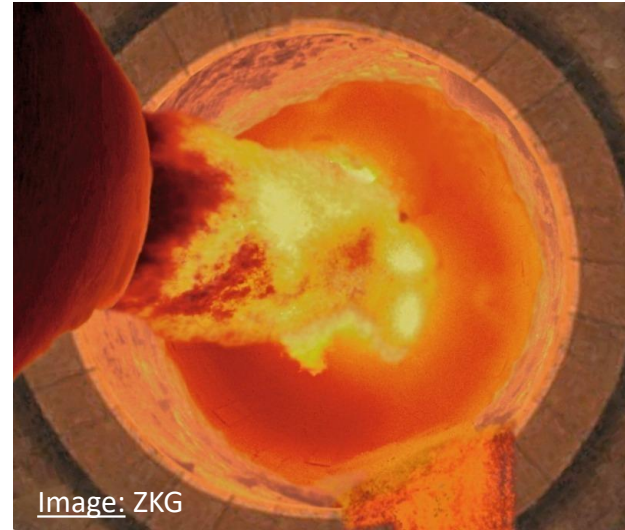
Lab scale vs. full-industrial scale

Sandia Flame D



- Size and complexity
- Control of boundary conditions
- (Un)certainities
- Reproducibility /representability
- Interaction with the product, e.g. heat transfer, process emissions, ...
- Accessibility for (advanced) measurement techniques
- Cost, risk, time and logistics
- Documentation

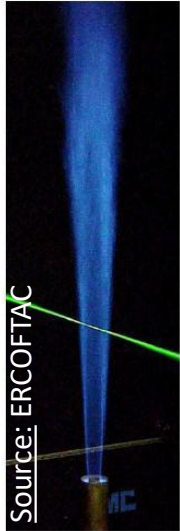
Rotary furnace



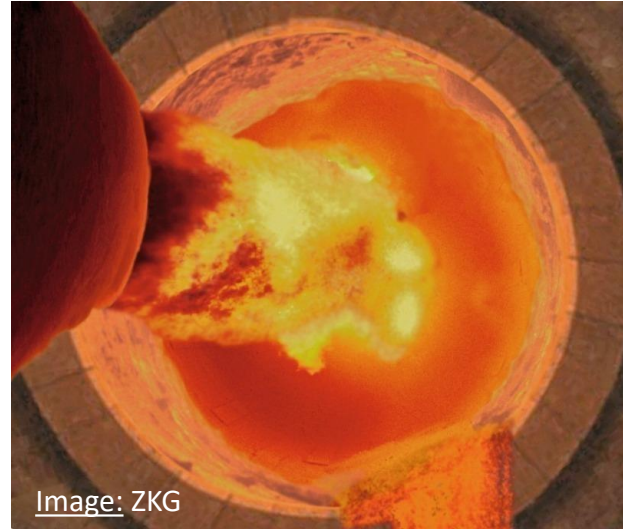
Lab-scale experiments are specifically designed to investigate certain phenomena, and simplified accordingly. With industrial systems, you take what you get...

Lab scale vs. full-industrial scale

complexity, uncertainty, cost, risk, ...



- Size and complexity
- Control of boundary conditions
- (Un)certainities
- Reproducibility /representability
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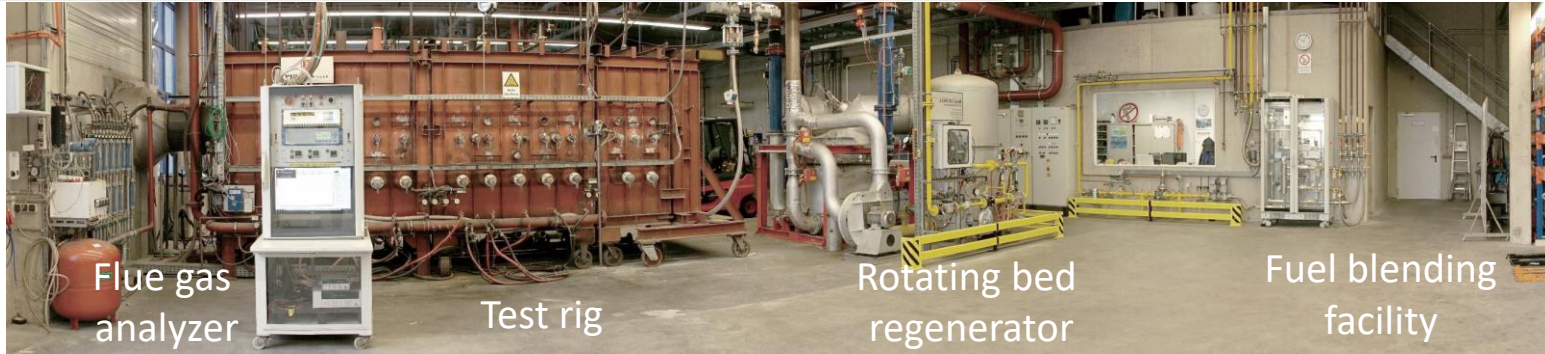


control of boundary conditions, data resolution (time & space),
reproducibility, accessibility, ...

Definitions – a proposal for applied combustion research

- **Lab scale:** experiments **designed specifically** to investigate **well-defined** physical/chemical **phenomena**. Focus on good control over the boundary conditions, reproducibility and accessibility with (advanced) measurement techniques.
- **Industrial scale:** The actual application, **as it is found in industry**. Focus on fitness for purpose, safety, product quality (where applicable), efficiency, pollutant emissions, CAPEX/OPEX, ...
- **Semi-industrial scale:** experiments designed to **recreate the crucial features** of an industrial process on a **smaller scale**, with some **simplifications**. Focus on reasonable **accessibility** for measurement techniques, good control over **boundary conditions** and **reduced cost** and **risk**.

An example of a semi-industrial combustion test rig (GWI Test Rig No. 1)

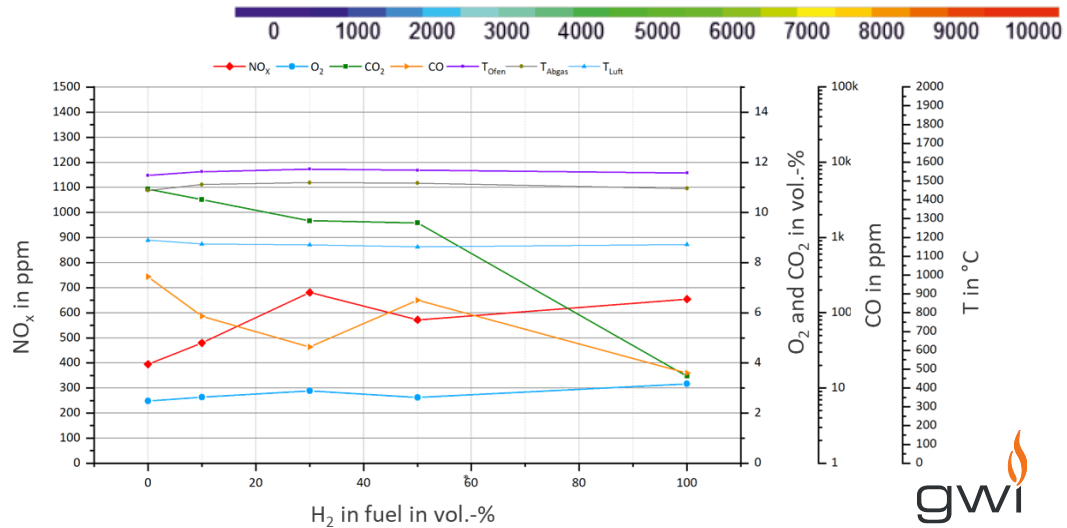
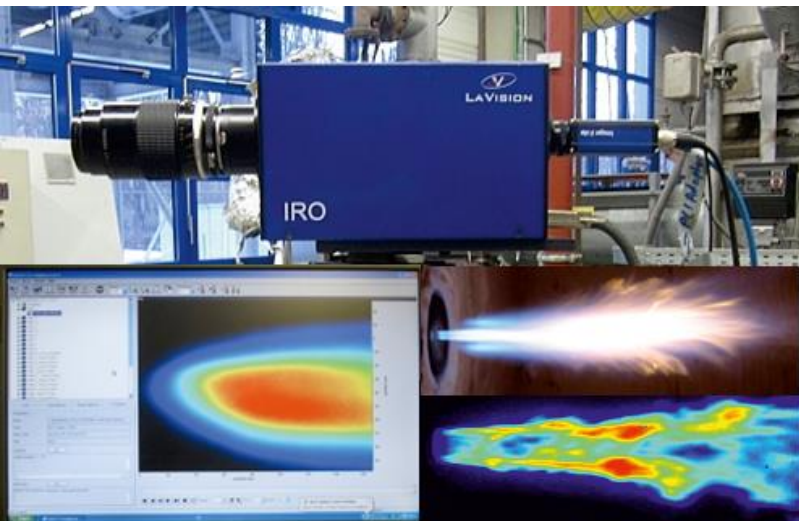
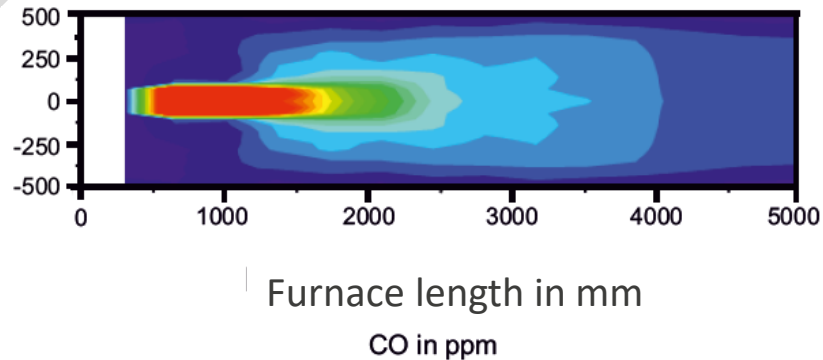
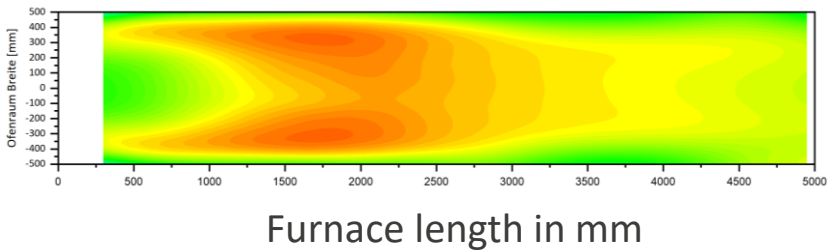


Key features:

- Maximum firing rate: 1.3 MW
- Maximum wall temp.: 1,600 °C
- Maximum air preheating: 1,250 °C
- Oxy-fuel capable up to 400 kW
- Fuel flexibility (gases), H₂ supply up to 1 MW
- Flexible geometry
- Good accessibility for measurements
- Heat-up time: about 12 h



Experimental data from semi-industrial test rigs



Do we still need semi-industrial testing anyway?

What about Computational Fluid Dynamics?

CFD... or why bother with semi-industrial experiments anymore?

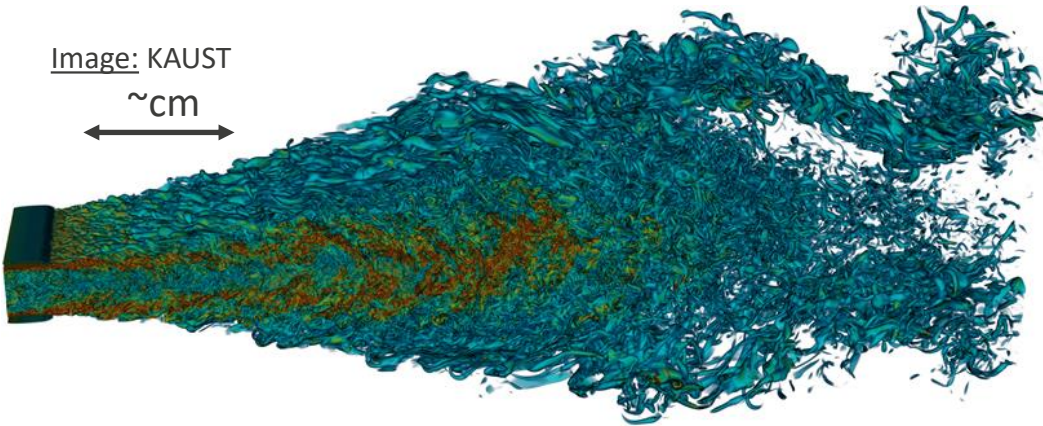
- In recent years, **CFD modeling** has become a powerful tool, both for **fundamental research** and **industrial application**, across many fields.
- In principle, CFD could be the ideal tool to **bridge the gap** between lab-scale experiments and full-scale application, offering **high data resolution** at **full scale, without interfering** in the actual process.
- But some challenges and constraints remain, such as:
 - **Boundary conditions** in industrial CFD can often be quite uncertain or „best guesses“.
 - **Trust?** It's just numbers in a computer, after all...
 - Scales are **still an issue**: turbulent scales (e. g. Kolmogorov vs. integral turbulent scales), chemical time scales,
Scale-resolving simulations can lead to **extreme hardware requirements**.

Simulations have scale issues too, ...

DNS of a combustion process in a gas turbine combustion chamber

Image: KAUST

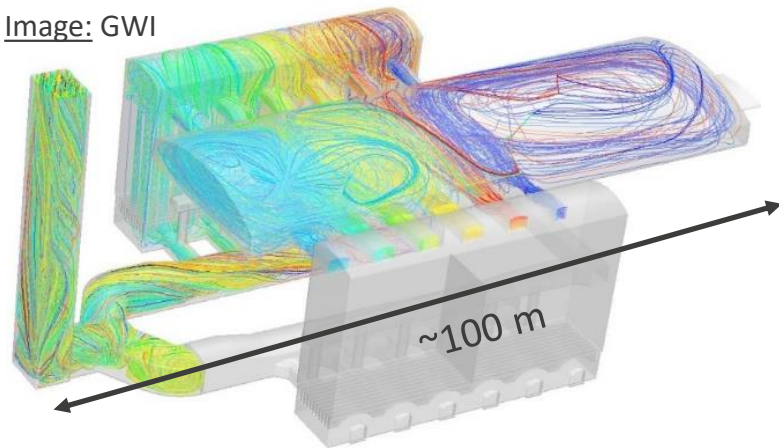
~cm



- Premixed CH_4 /air combustion, gas turbine conditions
- **22 billion cells**, transient, 4 TB per time step

CFD simulation (RANS) of a regenerative glass melting furnace (100 MW)

Image: GWI

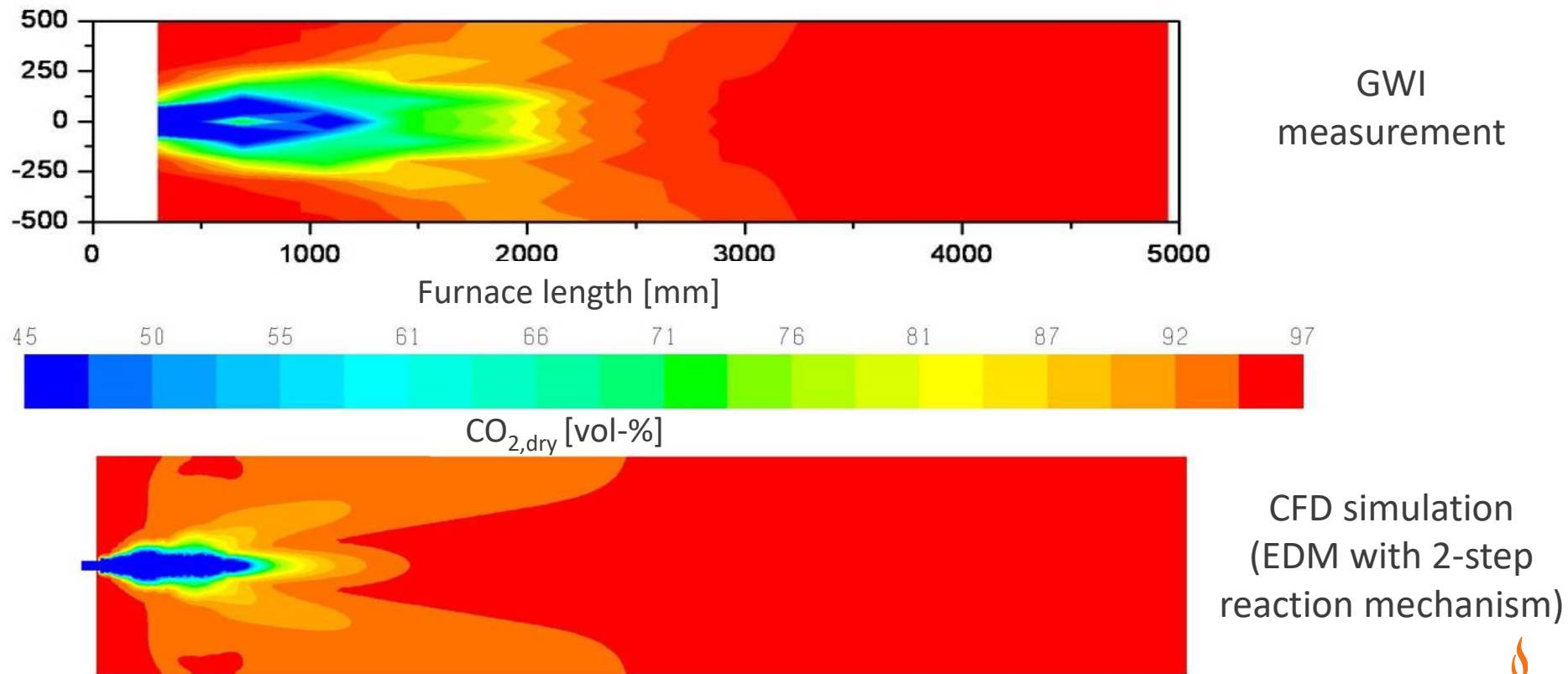


- Non-premixed natural gas/air combustion, air preheating: 1,200 °C
- About **10 million cells**, steady-state file size: a few **GB** in total

Validating CFD modeling

- CFD methods suited to describe combustion phenomena in great detail (e.g. DNS, LES, DES) may be **too computationally expensive** to describe full-scale applications. Simplified, less expensive approaches, e. g. **steady-state RANS**, may be necessary.
- Also, the **purpose** of the simulations may vary: **design/optimization** vs. **fundamental analysis**.
- Any CFD simulation is only as good as the **numerical mesh** it is based on, the **models** and the **solver** that it uses and the **boundary conditions** that are provided. Each of these aspects introduces **errors** and **uncertainties**.
- **Validation** using data from **semi-industrial test rigs** is useful to check whether a chosen CFD modelling approach is suitable to describe a full-scale industrial process at all, and to **assess** the **uncertainties** involved.

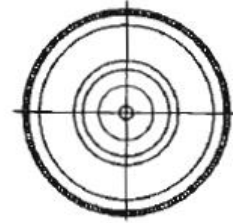
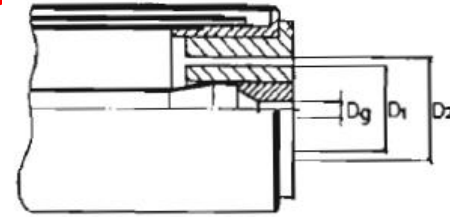
Measurement vs. simulation: oxy-fuel combustion of natural gas (400 kW)



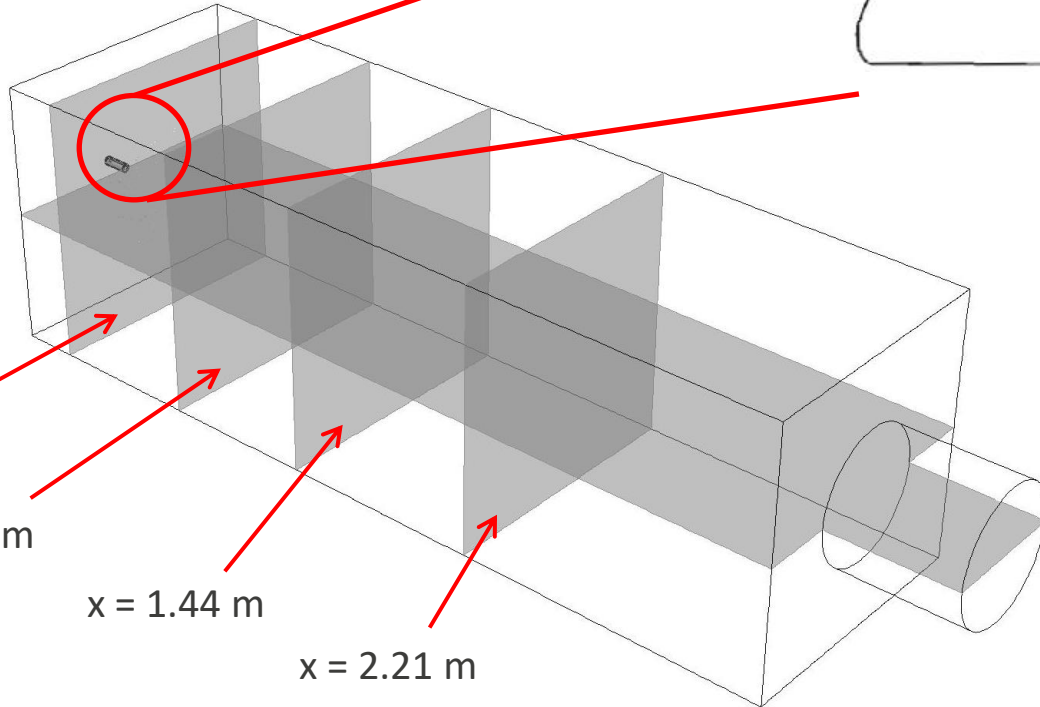
OXYFLAM experiments at IFRF research station, Ijmuiden (NL)

L x W x H:

3440 mm x 1050 mm x 1050 mm



D_g : 4 mm
 D_1 : 28 mm
 D_2 : 36 mm



Source: Lallemand, N, Dugué, J., Weber, R.,
"Analysis of the Experimental Data Collected
during the OXYFLAM-1 and OXYFLAM-2
Experiments - Part One", IFRF Report F85/Y/4,
Ijmuiden, NL, 1997

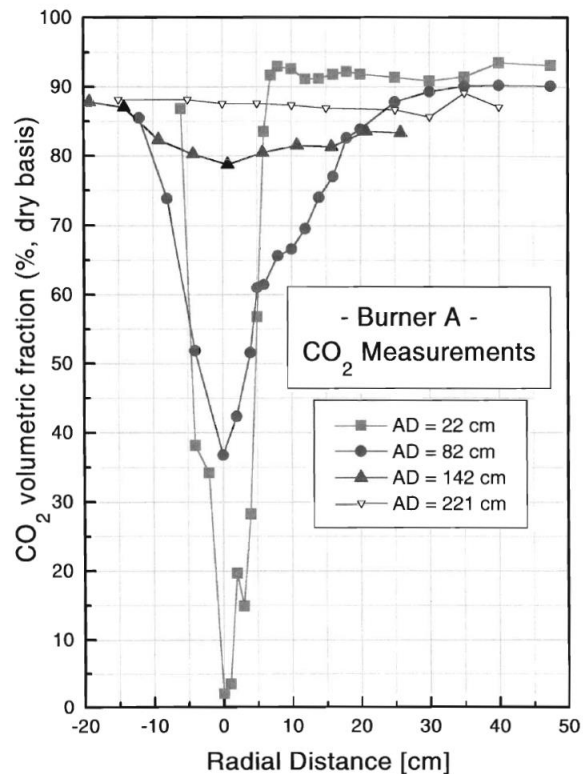
Models and boundary conditions

- CFD code: ANSYS Fluent, steady-state RANS
- Mesh: 1.7 Mio. cells, hybrid, full-3D
- Turbulence model: Realizable k- ϵ
- Combustion model: non-adiabatic PDF-Equilibrium-Model
- Radiation model: Discrete-Ordinates-Model
- Thermal boundary condition at furnace walls (based on measurements):

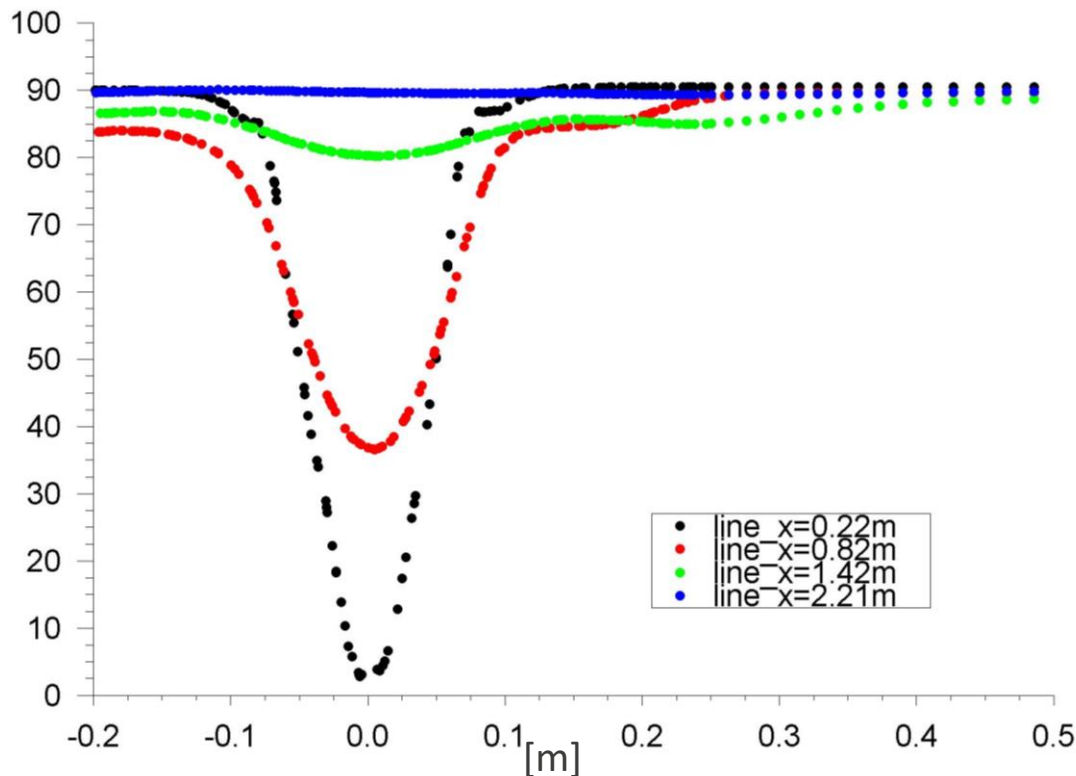
$$\dot{q} = 35 \frac{kW}{m^2}$$

Firing rate	780 kW
λ (100 % O ₂)	1.03
Natural gas composition:	
CH ₄ [vol.-%]	86.0
C ₂ H ₆ [vol.-%]	5.4
C ₃ H ₈ [vol.-%]	1.87
C ₄ H ₁₀ [vol.-%]	0.58
C ₅ H ₁₂ [vol.-%]	0.14
N ₂ [vol.-%]	4.01
CO ₂ [vol.-%]	1.79
O ₂ [vol.-%]	0.21

Measurement vs. simulation: CO₂ profiles (Oxy-fuel)

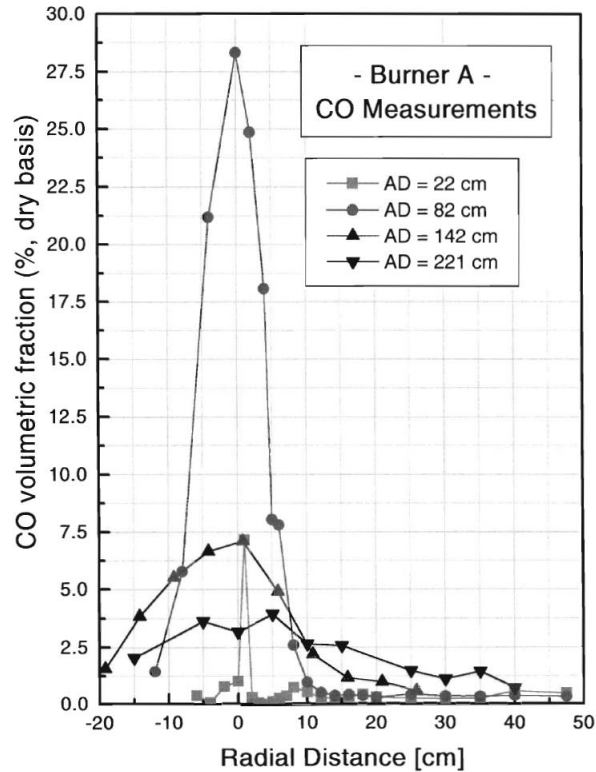


IFRF measurements

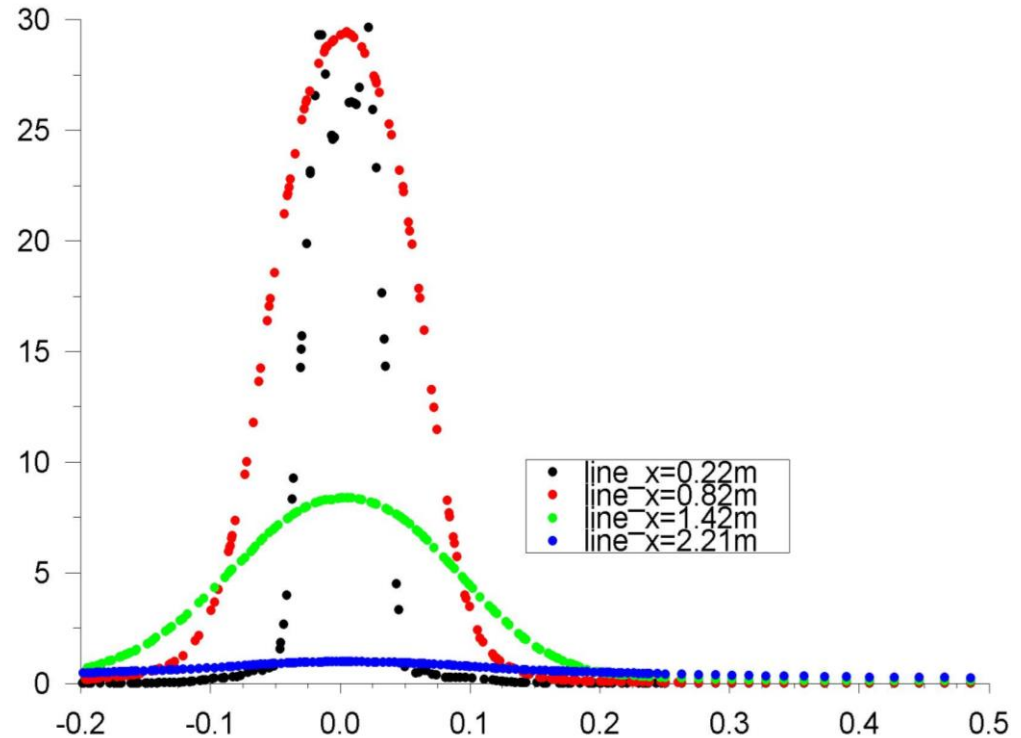


CFD simulation (GWI)

Measurement vs. simulation: CO profiles (Oxy-fuel)

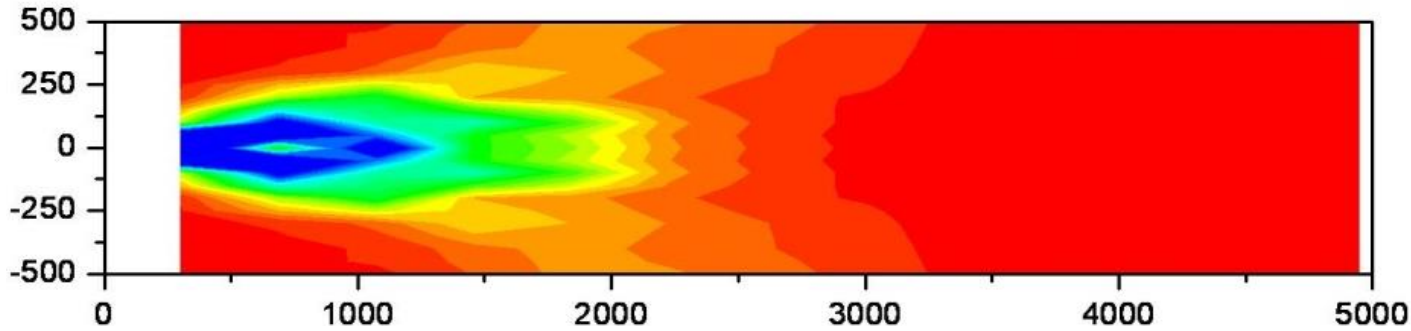


IFRF measurements

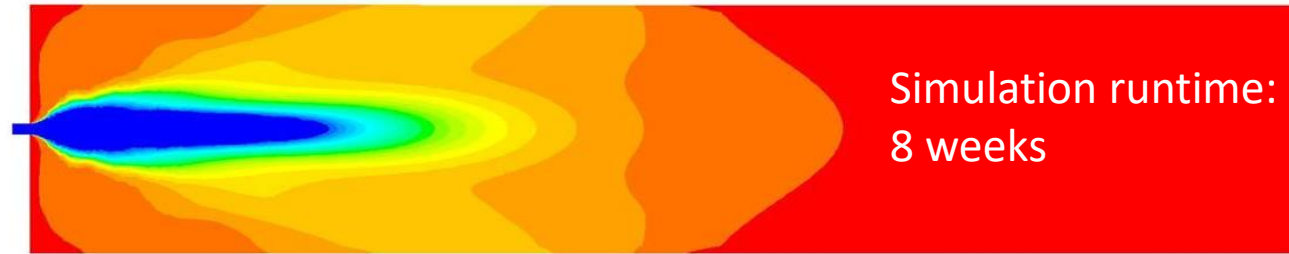


CFD simulation (GWI)

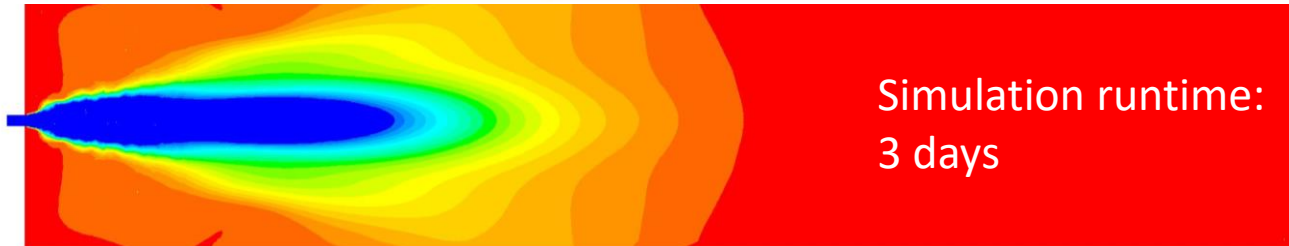
Measurement vs. simulation: oxy-fuel combustion



GWl measurement



CFD simulation
(EDC
17 species)



CFD simulation
(non-adiabatic
PDF equilibrium)



Measurements and simulations in industrial-scale applications

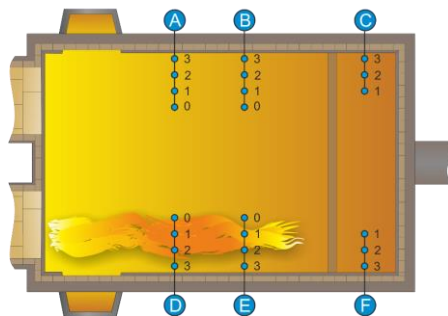
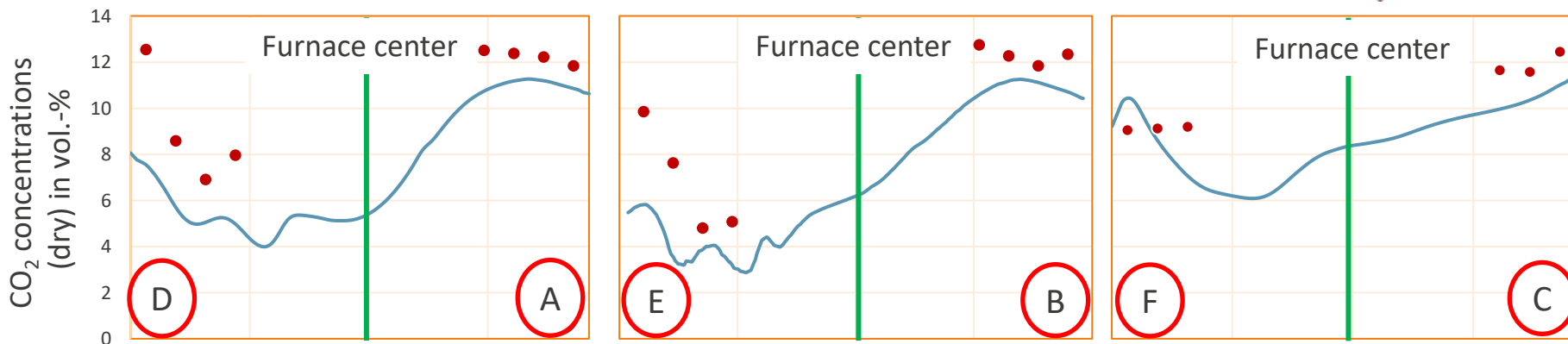


Image: GMIC



— Simulation ● Measurement

Higher CO₂ concentrations in measurements due to process emissions!

The future...

New topics and new methods?

Future developments

- Many energy-intensive industries are faced with **new challenges**, such as:
 - Decarbonization (=> new fuels, electrification and/or hybrid systems)
 - Energy (in)security
 - Digitalization
- At the same time, new tools and methods are becoming available to the industrial sectors, often driven by „**Big Data**“ methods: Artificial Intelligence, Artificial Neural Networks (ANN), Digital Twins, Machine Learning, ...
- Many of these new approaches more or less **forego physical modelling** and rely instead on **statistical analysis techniques** and **huge data sets** for **specific plants**. This may limit their usefulness for **extrapolation** to „new“ operational conditions, e. g. using hydrogen instead of natural gas.

New topics require lab-scale experiments, ...

Some things are better tried on a small scale first :



NH₃/H₂ combustion:

P: 8 kW

λ : 1.05

Various Swirl Numbers:

$0 < S < 1.1$

Further info:

ECM 2023

Poster # 436074, Room 4,

Wednesday morning

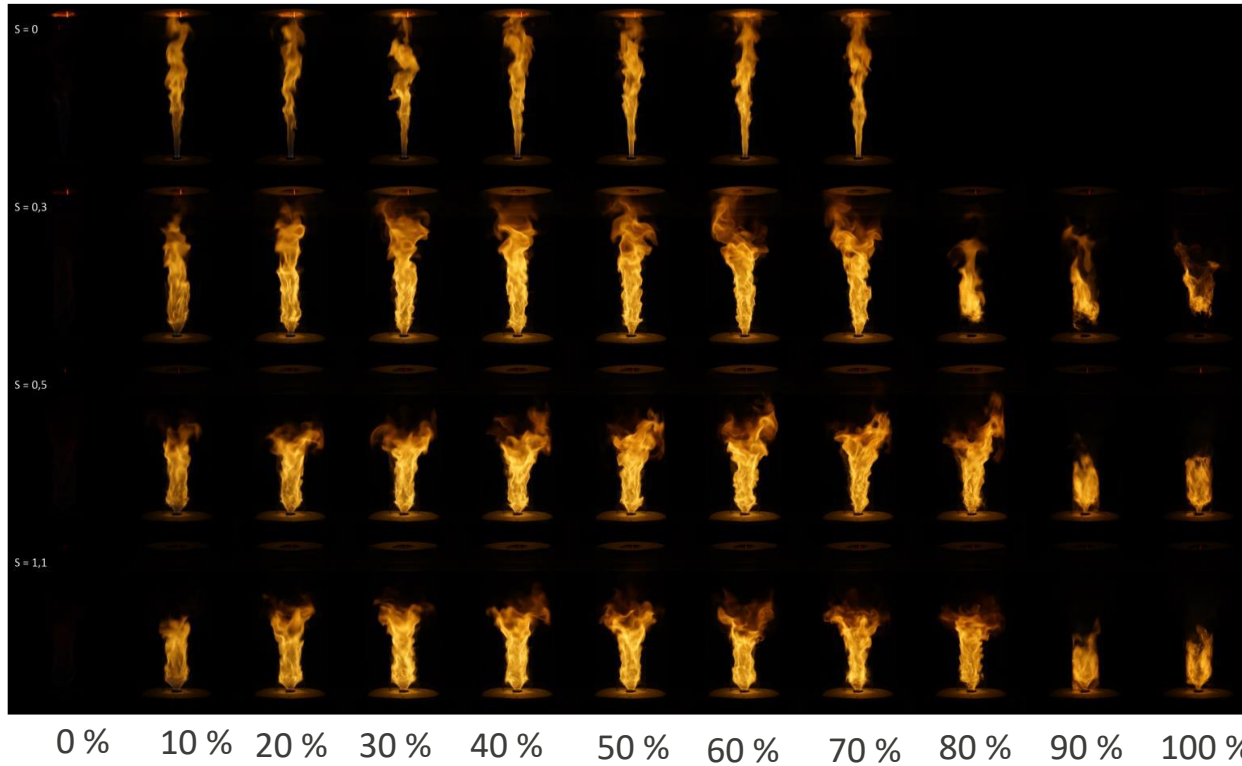
(Session #1)

Contact: M. Biebl

marcel.biebl@gwi-essen.de

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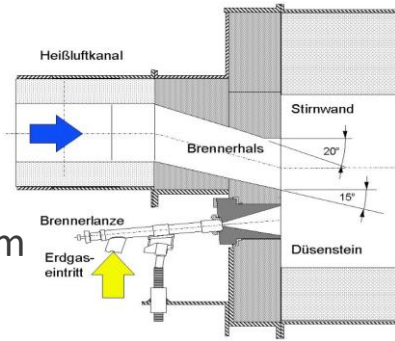
marcel.biebl@gwi-essen.de

...semi-industrial test rigs, ...

Project **HyGlass**: Investigating hydrogen-fired glass melting on a semi-industrial scale

Underport configuration

Preheated air
(1,150 °C)



Variable momentum
fuel lance

$P = 500 \text{ kW}$; $\lambda = 1.1$
(constant in all experiments)

GWl HT burner test rig



H₂ supply by trailer



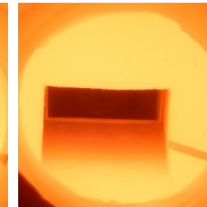
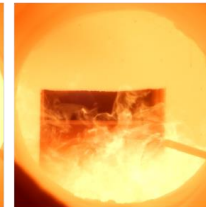
NG

10 % H₂

30 % H₂

50 % H₂

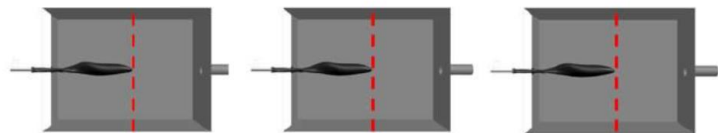
100 % H₂ (by volume)



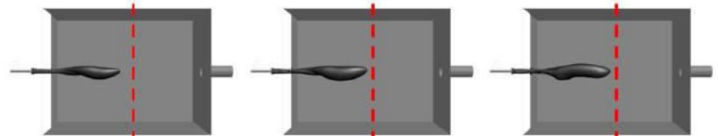
.... CFD simulations, ...

Simulation of the impact of H₂ admixture on an industrial burner (100 kW) in a test rig

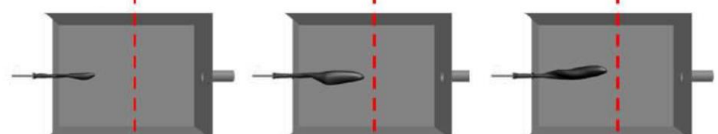
Natural gas



10 % H₂



50 % H₂



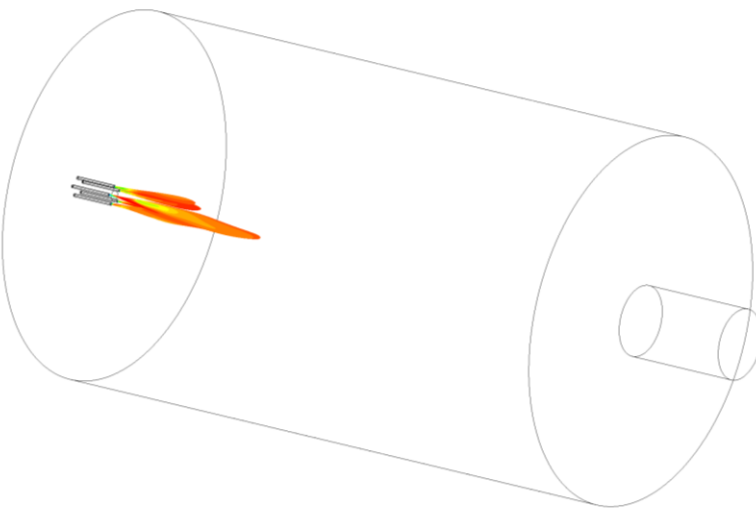
$V_{\text{gas}} = \text{const}$
 $V_{\text{air}} = \text{const}$

$V_{\text{gas}} = \text{const}$
 $\lambda = \text{const}$

$P = \text{const}$
 $\lambda = \text{const}$

Oxy-fuel combustion of hydrogen in an
3.5 MW aluminum scrap recycling furnace

T in °C



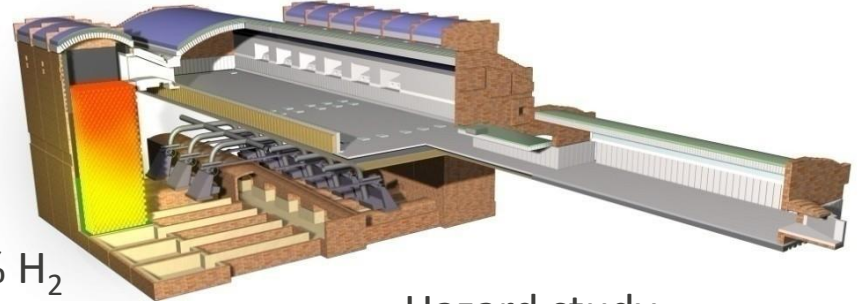
Flame shape visualized
with iso-surface of the stoichiometric
mixture fraction

Images: GWI

... and full-scale industrial trials (HyNet/HyDeploy, NSG, 2022)*

- Investigations on the impact of hydrogen on an industrial float glass plant (50 MW) in UK.
- 3 weeks of testing (6 h each) on **1 port**, from 20 % to **100 % H₂**. 5-day-long test run at 15 % H₂ on **all ports**.
- **Logistics** is a challenge: at 100 % H₂, 1 trailer had to be replaced every 40 min. Sufficient H₂ (and trailers!) have to be available for full-scale tests.
- **Safety-compliant handling** of large amounts of H₂ for testing purposes in an industrial plant is not easy.

Image: CGE Glass



Hazard study

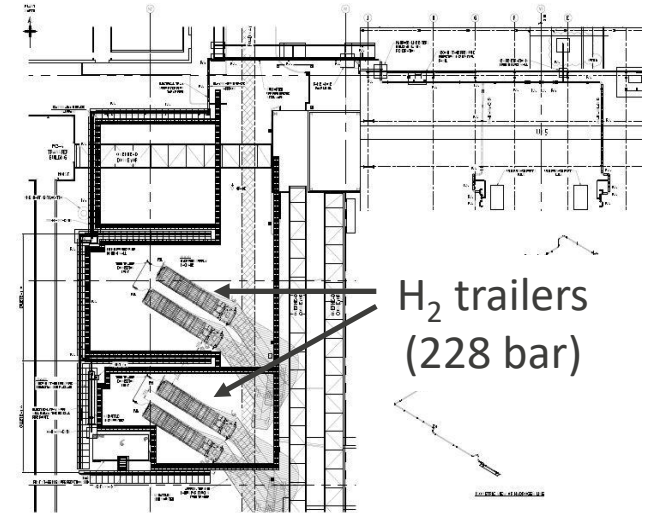


Image: NSG

*Keeley, A., Hydrogen Combustion on a Float Glass Furnace, ICG 2022, Berlin, Germany

Conclusion

- **Scales matter** in combustion research, both because of the **significant differences** in various end-use applications, but also because the **physical and chemical phenomena** themselves.
- Semi-industrial experiments serve to **bridge the gap** between fundamental combustion investigations and full-scale industrial applications, minimizing cost and risk for R & D.
- CFD modeling will likely **not completely replace** semi-industrial testing, but rather **complement** it, as both approaches have their **respective benefits** and **drawbacks**.
- A **combined approach** using lab scale experiments, semi-industrial tests and CFD can help **reduce the risks** and provide **valuable information** when implementing new technologies on an industrial scale.

“Nobody trusts a computer simulation except the guy who did it, and everybody trusts experimental data except the guy who did it.

Why not combine the two and get results everybody can mistrust a little.”

T. Kordyban

„In theory, there is no difference between theory and practice. But in practice, there is.“

Walter J. Savitch (1923 - 2021)

Thank you for your attention

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